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THE INFLUENCE OF THIN BENZOATE-DOPED POLYANILINE COATINGS ON CORROSION PROTECTION OF MILD STEEL IN DIFFERENT ENVIRONMENTS

Branimir Z. Jugović[1,*], Ali R. Elkais[2,3], Milica M. Gvozdenović[2], Branimir N. Grgur[2]

[1]Institute of Technical Sciences of the Serbian Academy of Sciences and Arts, Knez Mihailova 35/IV, 1100 Belgrade, Serbia
[2]Faculty of Tecnology and Metallurgy, University of Belgrade, Karnegijeva 4, 11120 Belgrade, Serbia
[3]University of Elmergib Chemical Engineering Department, El-Khums, Libya

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Abstract

The corrosion process of mild steel in the presence of benzoate-doped polyaniline coatings exposed to 3% NaCl has been investigated. This system was also tested for cathodic protection and it has proven more efficient comparing to mild steel alone.

1. Introduction

Mild steel is undoubtedly the cheapest and the most commonly used construction material. It has been extensively used for centuries in many areas, for water pipes, boats, docks, tanks, vessels, etc. Because of its low nobility and structural defects, mild steel, in contact with other metals, corrodes practically in all environments [1].

The application of electroconducting polymers is a relatively new approach in corrosion protection of mild steel in different environments [2-4]. These polymers show a semimetallic conductivity, and yield different effects when applied on metals, especially on mild steel. This is abundantly evidenced in literature, indicating a beneficial corrosion protection of many metals and alloys in different corrosion environments in the presence of conducting polymer-based coatings. Since the mid-1980s, numerous studies have shown that polyaniline-, polypyrrole-, or polythiophene-based coatings lower the corrosion rate of mild steel, stainless steel, aluminum, and copper [2,3]. The conducting polymer can either be applied as a neat coating or as dispersion in a polymer binder [4].

Polyaniline (PANI) is probably the most thoroughly investigated conducting polymer in corrosion protection of mild steel [3] It has been observed, though it is not well investigated, that, unlike regular organic coatings, PANI can protect metal under a scratched or damaged coating surface [5,6]. Many different mechanisms explaining the role of PANI in metal protection have been proposed [3,7-9]. Unfortunately, the mechanism of corrosion protection is still elusive.

Electrochemically deposited benzoate-doped PANI films exhibit good anticorrosion performances for mild steel, aluminum and copper in 3% NaCl, if applied either individually, or as primer with an epoxy topcoat [10-14].

The aim of this work has been to investigate the corrosion protection of mild steel in the presence of benzoate-doped PANI coatings in 3% NaCl as a model system, in order to investigate the possibility of a practical application of the proposed coating in cathodic protection.

2. Experimental

The electrochemical synthesis of PANI on mild steel (AISI 1212) electrodes was performed at a constant current density of 1.5 mA cm^{-2}, from an aqueous solution of 0.5 M Na

benzoate (p.a. Merck) and 0.25 M aniline (p.a. Aldrich). Prior to use, aniline was distilled in inert atmosphere. The electrolytes were prepared with doubly distilled water. The mild steel electrodes were mechanically polished with fine emery papers (2/0, 3/0 and 4/0, respectively), degreased in acetone and pickled in hydrochloric acid with addition of 0.5% urotropine (hexa-methylene-tetramine). Electrochemical experiments were carried out at ambient temperature, in three-electrode compartment cell with a saturated calomel electrode used as the reference and Pt wire as a counter electrode. The measurements were performed using PAR 273A potentiostat/galvanostat interfaced to PC.

The potential distribution along the mild steel sample during cathodic protection in 3% NaCl was investigated using the apparatuses shown on Fig. 1. The area of the exposed mild steel surface was 75 cm^2 (3 × 25 cm). The back side of the electrode was protected with a glued Plexiglas sheet. A titanium-coated ruthenium-oxide electrode with a surface of 1 cm^2 was used as an anode. The anode was placed near the mild steel sample, at the position denoted as $l = 0$.
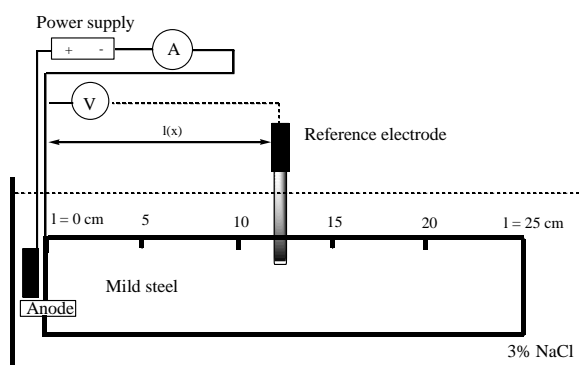

Figure 1. Schematic presentation of the apparatuses used for cathodic protection experiments.

3. Results

3.1. Electrochemical synthesis of benzoate-doped PANI film on mild steel

In Fig. 2, the anodic polarization curves of mild steel in 0.5 M Na benzoate solution and with 0.25 M aniline is shown. The corrosion potential of mild steel (E_{corr}) in pure 0.5 M Na-benzoate solution was –0.67 V. The active dissolution of mild steel occurred until the potential reached –0.5 V with the maximum current density of 0.6 mA cm^{-2}. At the potentials more positive than –0.45 V, passivation of the electrode occurred with the mean passivation current density of ~5 µA cm^{-2}. Transpassive regions accompanied by oxygen evolution were observed at potentials more positive than 1.25 V.

In the presence of aniline, the corrosion potential of the mild steel electrode was shifted positively, to the potential of –0.25 V. The electropolymerization of aniline on mild steel started at potentials more positive than 1 V, with a pronounced peak at 1.6 V.

The galvanostatic transient of the mild steel electrodes in pure 0.5 M Na benzoate solution with the addition of 0.1 and 0.25 M aniline was given in Fig. 3.
Without aniline in the solution, the potential-time curves had a relatively stable potential plateau, while the induction period was not observed. Applying the current density of 1.5 mA cm^{-2}, the potential increased from 1.3 to 2.25 V during 700 s. After that period, a sharp increase of the potential could be related to the formation of a non-conducting precipitate (e.g. iron benzoate) onto the electrode surface. With aniline in the solution, the polymerization was dependent on the aniline monomer concentration. In a 0.1 M aniline solution, a sharp increase of the potential after 120 s could be brought into relationship with the diffusion limitation of the aniline monomer. In the solution with 0.25 M of aniline, diffusion limitations were not

observed, while a slow increase of the potential, from 1 to 1.25 V, could be related to the polymerization of aniline.
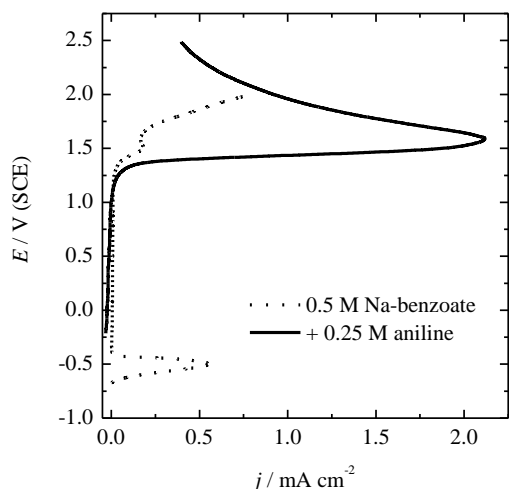

Figure 2. Anodic polarization curves ($v = 1$ mVs^{-1}) of mild steel in a 0.5 M sodium benzoate solution and with an addition of 0.25 M aniline monomer.
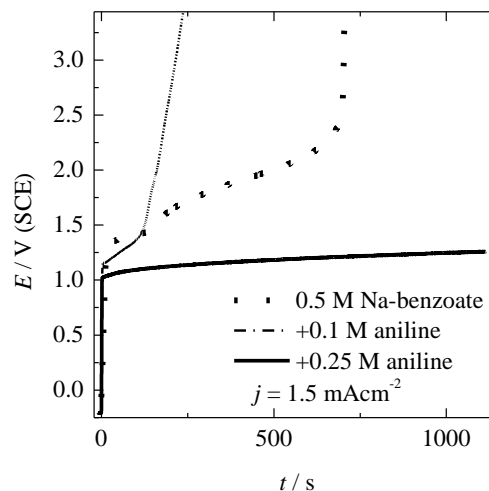

Figure 3. Galvanostatic transient of the mild steel electrodes in pure 0.5 M Na benzoate solution with 0.1 and 0.25 M aniline.

The obtained film was black, with good adhesion, determined by cracking. Assuming that the density of benzoate-doped PANI is 1.4 g cm^{-3} [15], and using the equation [16]:

$$d = \frac{jt(M_m + yM_a)}{(2+y)\rho F} \tag{1}$$

where M_m and M_a are the molar mass of the aniline monomer and benzoate anions, and y the doping degree (the polymerization potential of 1.25 V suggests that PANI was in the pernigraniline form, $y = 1$), the thickness of the PANI film has been estimated to be 6 μm.

Figure 4 shows cyclic voltammogram of the mild steel (MS)-PANI electrode in a pure 0.5 M Na-benzoate solution. In the anodic scan, in the potential region from –0.6 to 0.1 V, where doping with benzoate anions occurred, the current density was very small: ~ 1 μA cm^{-2}. The dedoping of benzoate anions occurred in the broad potential region, from 0.1 V to –0.7 V, and was probably overlapped with an oxygen reduction reaction. This means that the MS-PANI system is stable over a large potential range.
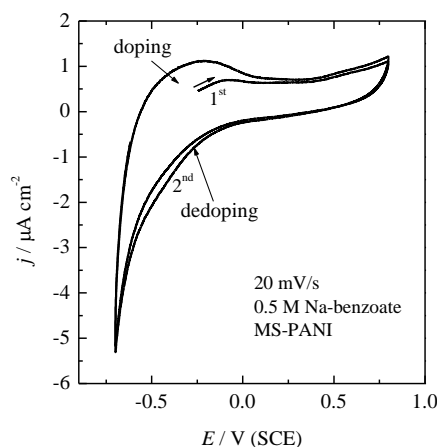

Figure 4. Cyclic voltammogram of the mild steel – PANI-benzoate electrode in a 0.5 M Na-benzoate solution.

3.2. Corrosion of mild steel and mild steel with electrochemically deposited benzoate-doped PANI film in 3% NaCl

The corrosion of mild steel in sea water (simulated with 3% NaCl) is very important for practical applications of this material; therefore, this type of corrosion has been investigated in this section of the study.

Figure 5 shows the polarization curves for mild steel and mild steel with benzoate-doped PANI in 3% NaCl. The anodic polarization curve for the mild steel electrode is characterized by a single slope (0.114 V dec^{-1}), while the cathodic curve is diffusion-controlled.
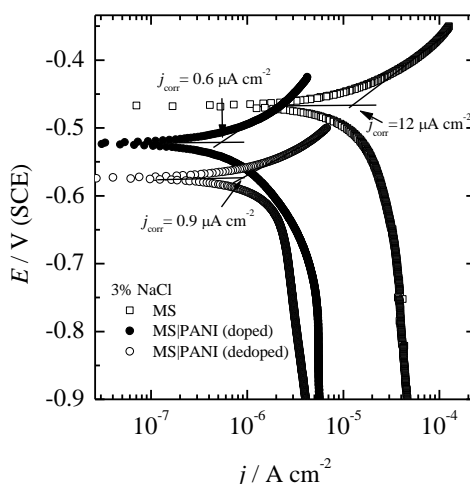

Figure 5. Potentiodynamic polarization curves ($v = 1$ mV s^{-1}) for mild steel and mild steel with a doped and de-doped PANI film in 3% NaCl.

The corrosion processes of mild steel is characterized by anodic dissolution of iron

$$Fe \rightarrow Fe^{2+} + 2e^{-} \qquad (2)$$

and the rate determining the mixed activation–diffusion-controlled cathodic oxygen reduction:

$$O_2 + 2H_2O + 4e \rightarrow 4OH^{-} \qquad (3)$$

The corrosion current density of 12 μA cm^{-2} for bare mild steel was obtained from the intercept of the anodic Tafel line with the corrosion potential ($E_{corr} = -0.466$ V).

After an hour-long immersion in 3% NaCl, the mild steel electrode with PANI in the doped state had a corrosion potential of -0.527 V, which is by 70 mV more negative than the corresponding value for a bare mild steel electrode. During the first sweep, the anodic curve had the similar slope as bare mild steel, while the cathodic curve, related to the oxygen reduction reaction and de-doping of benzoate anions, was characterized by a broad peak in the potential range from ~-0.6 V to ~-0.9 V. After the cathodic polarization (dedoping), the broad peak disappeared, as observed from the polarization curve recorded after the first cathodic sweep. After the cathodic polarization (de-doping), the corrosion potential was shifted to more negative values, $E_{corr} = -0.573$ V, characteristic for the dedoped state of polyaniline. It is interesting to note that the values of the corrosion current density for mild steel with a doped and dedoped PANI film were almost identical: 0.6 and 0.9 μA cm^{-2}, respectively.

3.3. Influence of PANI on the cathodic protection of mild steel

The corrosion of mild steel in sea water is mainly connected to the reduction of dissolved oxygen. The cathodic reaction in nearly neutral solutions is a diffusion-controlled oxygen reduction reaction (Eq. 3) and the anodic reaction is the dissolution of iron (Eq. 2),

The theory of cathodic protection is based on the fact that the corrosion potential (E_{corr}) has to be shifted cathodically by applying the current from an external power source that can ensure the minimal polarization to the 'reversible' potential, $E_r(Fe^{2+}|Fe)$ of iron in the solution, defined by the equation:

$$E_r(Fe^{2+}|Fe) = -0.683 + 0.029 \log 10^{-6} \quad (vs \text{ SCE}) \tag{4}$$

This minimal polarization, ΔE_{min}^p, is usually ~0.2 V, as it can be seen in Fig. 6. Under such conditions, the dissolution of iron is practically eliminated, and only oxygen reduction occurs on the surface of mild steel. Since corrosion is more efficiently inhibited when polarization is higher, polarization should be as high as 0.45 V. After that, a hydrogen evolution reaction may occur at the potential of ~ −1.1 V vs SCE, E_{max}^p, which can provoke hydrogen penetration into the metal structure and cracking corrosion. Accordingly, the optimum current for mild steel protection should shift the potential of 0.2 V below the corrosion potential and to approximately −1.1 V vs SCE. In Fig. 6, the experimental polarization curve of mild steel in 3% NaCl and the theoretical curves of possible corrosion reactions are shown.
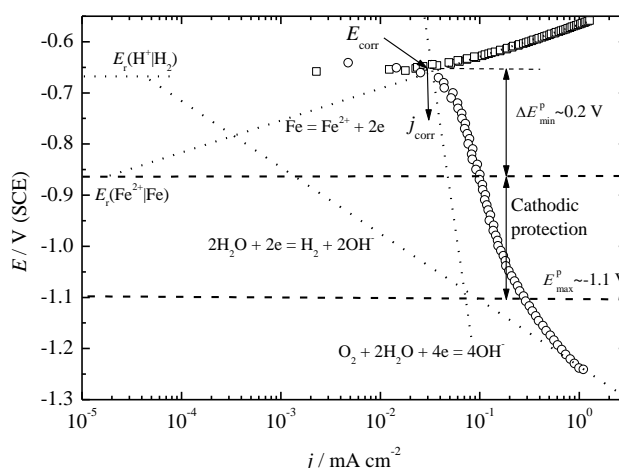

Figure 6. Polarization curve of the mild steel electrode in a 3% NaCl solution, with the theoretical lines of possible corrosion reactions.

The main idea underlying the following experiments has been to investigate the influence of a benzoate-doped PANI film in cathodic protection and in the event of a failed cathodic protection. The mild steel sample was exposed to a 3% NaCl solution. After the stabilization of the corrosion potential, the distributions of the potential along the mild steel sample were measured, for different currents; the results are shown in Fig. 7.

As it can be seen in Fig. 7, for the current densities of 20 and 30 mA, at the position $l = 0$ and 5 cm, the potential is below the line where a hydrogen evolution reaction is likely to occur. For the current density of 10 mA, the potential at 25 cm is near ΔE_{min}^p. Therefore, an optimal current which meets the requirements for an efficient cathodic protection is ~15 mA ($j = 0.2$ mA cm^{-2}).

The experiment shown in Fig. 7 was repeated with a mild steel electrode partially covered with PANI and the results are shown in Fig 8.

It can be observed that the MS-PANI system requires a lower cathodic protection current, e.g. 10 mA (0.13 mA cm^{-2}) or even lower than a bare mild steel electrode. This means that the power consumption would be more than 30% lower than for a bare mild steel electrode.
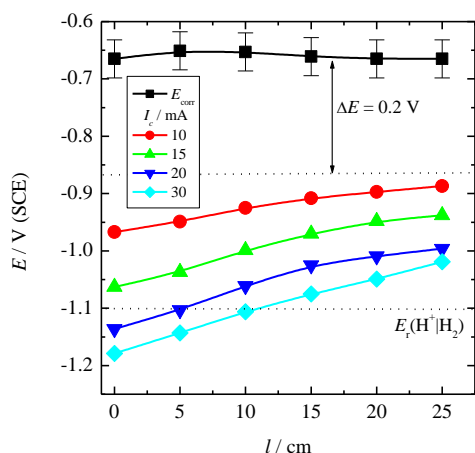
Figure 7. Dependence of the potential along The mild steel electrode for different currents in a 3% NaCl solution.
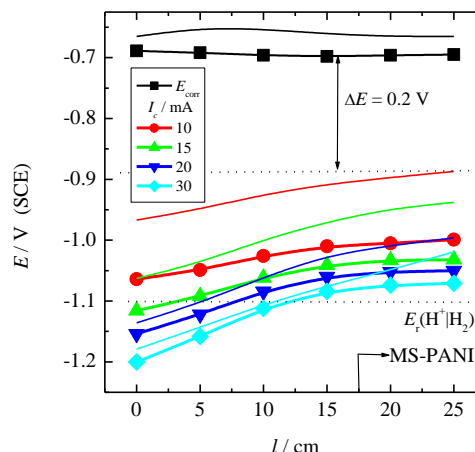
Figure 8. Dependence of the potential along the mild steel electrode partially covered with PANI for different currents in 3% NaCl solution; the lines represent the data from Fig 7.

Figure 9 shows a comparison of the samples after a ten-hour immersion in 3% NaCl at the corrosion potential (simulating cathodic protection failure). It is obvious that mild steel partially covered with benzoate-doped PANI showed extraordinary protection of mild steel in the case of cathodic protection failure in a 3% NaCl solution.

Figure 9. Comparison of the images of bare mild steel and mild steel with partial PANI-benzoate coatings after a ten-hour exposure to 3% NaCl at the corrosion potential.

5. Conclusion

The corrosion of mild steel with partial PANI-benzoate coatings in three different environments (3% NaCl, atmosphere and the Sahara sand) has been investigated. It has been concluded that in all of the tree investigated environments, benzoate-doped PANI coatings could protect mild steel even when the coatings are partially applied for a limited period of time. It has also been shown that partial benzoate-doped PANI coatings could protect mild steel in the case of cathodic protection failure. Based on the experimental evidence, the 'switching zone mechanism' has been proposed and discussed in detail.

Acknowledgment:

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